

SIZE OF CONDENSATE NUCLEI IN A STREAM  
OF SUPERSATURATED VAPOR

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UDC 536.423.4

Analyzed is the effect of the relative vapor stream velocity on the size of condensate nuclei.

Many studies have been published so far [1-3 et al.] concerning the size of condensate nuclei in stationary supersaturated vapor. The results of these studies can be used for analyzing the process of initial phase transformation in a vapor stream, of course, but only under the condition that the relative velocity between the phases is zero.

In practice one usually encounters problems of condensation in a vapor stream where droplets move relative to it. Quite understandably, the conditions of the vapor flow cannot but affect the kinetics of condensation. It has been shown in [4] that an important factor in the process of homogeneous condensation is the mean free-flow-time of a droplet. This mean free-flow-time will be defined as the mean time during which a droplet moves without colliding against vapor molecules, i.e., the time between two successive collisions of a droplet containing  $g$  molecules against single vapor molecules.

We will determine the mean free-flow-time  $\tau_g$  of a droplet whose radius is  $r_g$  and which consists of  $g$  molecules, the radius of each molecule being  $r_1$ , when  $g \gg 1$  and the relative velocity of the vapor stream is  $V_{1g}$ . For the purpose of analysis, we consider separately a fictitious spherical surface (Fig. 1) with the radius

$$r = r_g + r_1,$$

representing the effective collision surface between a droplet complex (radius  $r_g$ ) and a vapor molecule (radius  $r_1$ ), and we calculate the number of collisions between vapor molecules and this surface per unit time.

The surface of the hemisphere facing the vapor stream ( $0 \leq \theta \leq \pi/2$ ) will be denoted by  $S_+$ , the back surface ( $\pi/2 \leq \theta \leq \pi$ ) will be denoted by  $S_-$ . Elementary spherical zones on the front surface and on the back surface will be denoted by  $dS_+$  and  $dS_-$ , respectively. The area of such an elementary zone on the given spherical surface is

$$dS = 2\pi r^2 \sin \theta d\theta. \quad (1)$$

Let us determine the number of molecules  $dn_+$  colliding against an elementary surface element  $dS_+$  per unit time. According to [5], we can write

$$dn_+ = n_1 \frac{V_m}{2 \sqrt{\pi}} \{ \exp(-\eta_n^2) + \sqrt{\pi} \eta_n [1 + \operatorname{erf}(\eta_n)] \} dS_+. \quad (2)$$

Analogously, the number of collisions  $dn_-$  against a surface element  $dS_-$  is

$$dn_- = n_1 \frac{V_m}{2 \sqrt{\pi}} \{ \exp(-\eta_n^2) - \sqrt{\pi} \eta_n [1 - \operatorname{erf}(\eta_n)] \} dS_-. \quad (3)$$

Here

$$V_m = \sqrt{\frac{2kT}{m_1}}$$

Translated from *Inzhenerno-Fizicheskii Zhurnal*, Vol. 24, No. 1, pp. 53-58, January, 1973. Original article submitted August 10, 1971.

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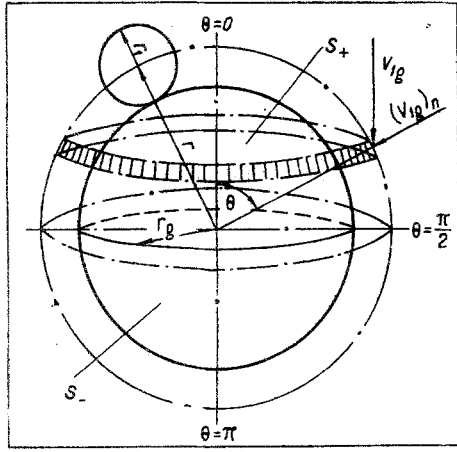


Fig. 1

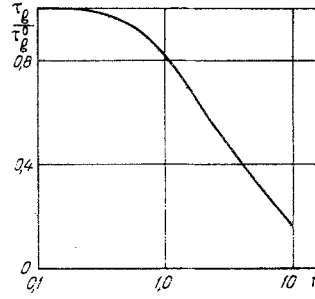


Fig. 2

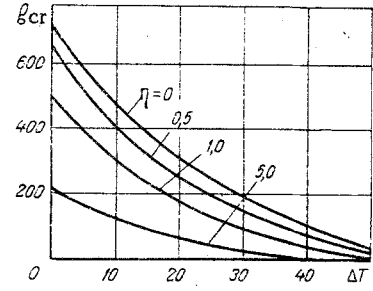


Fig. 3

Fig. 1. Diagram to show effective section through a colliding system (fictitious spherical surface).

Fig. 2. Variation in the relative mean free-flow-time of a droplet.

Fig. 3. Number of molecules in a condensate nucleus, as a function of the degrees subcool  $\Delta T$  ( $^{\circ}\text{K}$ ) in water vapor.

is the most probable thermal velocity of vapor molecules. The quantity

$$\eta_n = \frac{(V_{1g})_n}{V_m}$$

characterizes the ratio of two velocities: the component of the relative vapor velocity  $(V_{1g})_n$  normal to the surface element and the most probable thermal velocity of vapor molecules  $V_m$ .

The error function in (2) and (3) is

$$\text{erf}(\eta_n) = \frac{2}{\sqrt{\pi}} \int_0^{\eta_n} \exp(-x^2) dx. \quad (4)$$

With the dimensionless relative vapor velocity

$$\eta = \frac{V_{1g}}{V_m} = \eta_n \frac{V_{1g}}{(V_{1g})_n},$$

we can write

$$\eta_n = \eta \cos \theta. \quad (5)$$

Having thus determined the number of collisions  $n_+$  and  $n_-$  between vapor molecules and surfaces  $S_+$ ,  $S_-$ , respectively, we find the total number of collisions

$$n = n_+ + n_-. \quad (6)$$

In order to determine  $n_+$  and  $n_-$ , it is necessary to integrate expressions (2) and (3) with respect to  $S_+$  and  $S_-$ , respectively. Taking into account (1) and (5), we obtain

$$n_+ = n_1 \sqrt{\frac{2kT}{\pi m_1}} \pi r^2 F_+(\eta), \quad (7)$$

$$n_- = n_1 \sqrt{\frac{2kT}{\pi m_1}} \pi r^2 F_-(\eta), \quad (8)$$

where

$$F_+(\eta) = \frac{\sqrt{\pi}}{2} \cdot \frac{\text{erf}(\eta) + \eta^2 + 2 \int_0^{\eta} x \text{erf}(x) dx}{\eta}, \quad (9)$$

$$F_-(\eta) = \frac{\sqrt{\pi}}{2} \cdot \frac{\operatorname{erf}(\eta) - \eta^2 + 2 \int_0^\eta x \operatorname{erf}(x) dx}{\eta}. \quad (10)$$

With the aid of these relations, it is not difficult to determine the total number of molecules colliding against a droplet per unit time:

$$n = n_1 \sqrt{\frac{8kT}{\pi m_1}} \pi r^2 F(\eta), \quad (11)$$

where

$$F(\eta) = \frac{1}{2} [F_+(\eta) + F_-(\eta)] = \frac{\sqrt{\pi}}{2} \cdot \frac{\operatorname{erf}(\eta) + 2 \int_0^\eta x \operatorname{erf}(x) dx}{\eta}. \quad (12)$$

When the relative vapor velocity  $V_{1g} = 0$ , then  $\eta = 0$  and function  $F(\eta) = 1$ . Under these conditions formula (11) becomes the well-known formula for the number of collisions between vapor molecules and a sphere of radius  $r_g$  in a stationary gaseous medium:

$$n_0 = n_1 \sqrt{\frac{8kT}{\pi m_1}} \pi r^2. \quad (13)$$

Knowing the number of collisions between a droplet and vapor molecules per unit time, we can easily determine the mean free-flow-time for a complex of  $g$  molecules:

$$\tau_g = \frac{1}{n} = \frac{1}{n_1 \sqrt{\frac{8kT}{\pi m_1}} \pi r^2 F(\eta)}. \quad (14)$$

When there is no relative motion, i.e.,  $\eta = 0$ , then formula (14) becomes the well-known formula for the mean free-flow-time of a droplet in stationary vapor:

$$\tau_g^0 = \frac{1}{n_1 \sqrt{\frac{8kT}{\pi m_1}} \pi r^2}. \quad (15)$$

With the aid of (14) and (15), we set up the ratios

$$\Phi(\eta) = \frac{\tau_g}{\tau_g^0}, \quad (16)$$

and

$$\Phi(\eta) = 1/F(\eta). \quad (17)$$

The trend of  $\tau_g/\tau_g^0$  as a function of  $\eta$  is well indicated by the curve in Fig. 2. As the dimensionless relative velocity of the vapor stream  $\eta$  increases, according to the graph, the quantity  $\tau_g/\tau_g^0$  decreases. For low relative vapor velocities ( $\eta \ll 1$ ) the first two terms in the Taylor series expansion of  $\operatorname{erf}(x)$

$$\operatorname{erf}(x) \approx \frac{2x}{\sqrt{\pi}} \left( 1 - \frac{x^2}{3} \right), \quad (18)$$

yield, after simple transformations,

$$\tau_g = \frac{\tau_g^0}{1 + \frac{1}{3} \eta^2 - \frac{2}{15} \eta^4}. \quad (19)$$

Formula (19) determines the mean free-flow-time of a droplet as a function of the relative vapor velocity at low values of  $\eta$ .

For high relative vapor velocities ( $\eta \gg 1$ ) the first two terms in the asymptotic series expansion of  $\text{erf}(x)$

$$\text{erf}(x) \approx 1 - \frac{\exp(-x^2)}{x \sqrt{\pi}}, \quad (20)$$

yield a hyperbolic relation

$$\tau_g = \frac{2}{\sqrt{\pi} \eta} \tau_g^0. \quad (21)$$

Let us now determine the critical size of a condensate nucleus under the given conditions. For this it is necessary to establish what number of molecules in a droplet  $g_{\text{cr}}$  will produce a dynamic equilibrium between incoming and outgoing molecules.

As has been shown in [4], a droplet consisting of  $g_{\text{cr}}$  molecules may be in dynamic equilibrium with the vapor when the probability  $p_-$  of one droplet molecule evaporating is equal to the probability  $p_+$  of one vapor molecule condensing. In accordance with the kinetic theory of liquids [1] and gases [5],

$$p_- \approx \frac{t}{\tau_g^*} \quad \text{and} \quad p_+ \approx \frac{t}{\tau_g}. \quad (22)$$

Here

$$\tau_g^* = \frac{\Delta}{\sqrt{\frac{8kT}{\pi n_1}}} \exp\left(\frac{U_g}{kT}\right) \quad (23)$$

is the mean time of interaction between vapor molecules and a droplet. It follows from (22) that a complex of  $g_{\text{cr}}$  molecules may be in dynamic equilibrium with the ambient vapor when the mean time of their interaction  $\tau_g^*$  becomes equal to the mean free-flow-time of the complex. The size of such a complex is determined by the number of molecules  $g_{\text{cr}}$  in it, namely

$$r_{\text{cr}} = 2r_1 \left[ \sqrt{\frac{1}{4\pi r_1^2 n_1} \cdot \frac{\Phi(\eta)}{\Delta}} \exp\left(-\frac{V_g}{2kT}\right) - \frac{1}{2} \right]. \quad (24)$$

Inserting into (24) the mean free-flow-path

$$\lambda_1 = \frac{1}{4\pi r_1^2 n_1}, \quad (25)$$

we obtain

$$r_{\text{cr}} = 2r_1 \left[ \sqrt{\frac{\lambda_1}{\Delta} \Phi(\eta)} \exp\left(-\frac{V_g}{2kT}\right) - \frac{1}{2} \right]. \quad (26)$$

The number of molecules in a droplet of critical size is then

$$g_{\text{cr}} = 8 \left[ \sqrt{\frac{\lambda_1}{\Delta} \Phi(\eta)} \exp\left(-\frac{V_g}{2kT}\right) - \frac{1}{2} \right]^3. \quad (27)$$

Unlike in [4], formulas (24) and (27) take into account the effect of the relative vapor velocity on  $r_{\text{cr}}$  and  $g_{\text{cr}}$ . For the condensation in a stationary medium ( $V_{\text{lg}} = 0$  and  $\eta = 0$ ) formulas (24) and (27) become directly the well-known formulas in [4].

The critical number of molecules  $g_{\text{cr}}$  as a function of degrees subcool  $\Delta T$  is shown in Fig. 3 for water vapor under a pressure of 0.5 bar and at various values of  $\eta$  from 0 to 5. The graph indicates that at each value of  $\eta$  the number of molecules in a condensate nucleus decreases as the degrees subcool increase. As the dimensionless relative velocity  $\eta$  increases, the number of molecules in a critical-size droplet decreases continually. For low relative velocities ( $\eta \ll 1$ ) Eqs. (12), (17), and (18) yield

$$r_{\text{cr}} = 2r_1 \left[ \sqrt{\frac{\lambda_1}{\Delta} \cdot \frac{1}{1 + \frac{1}{3}\eta^2 - \frac{2}{15}\eta^4}} \exp\left(-\frac{V_g}{2kT}\right) - \frac{1}{2} \right], \quad (28)$$

and

$$g_{cr} = 8 \left[ \sqrt{\frac{\lambda_1}{\Delta} \frac{1}{1 + \frac{1}{3} \eta^2 - \frac{2}{15} \eta^4}} \exp\left(-\frac{V_g}{2kT}\right) - \frac{1}{2} \right]^3 \quad (29)$$

For high relative velocities ( $\eta \gg 1$ ) Eqs. (12), (17), and (26) yield

$$r_{cr} = 2r_1 \left[ \sqrt{\frac{\lambda_1}{\Delta} \cdot \frac{2}{\pi\eta}} \exp\left(-\frac{V_g}{2kT}\right) - \frac{1}{2} \right] \quad (30)$$

and

$$g_{cr} = 8 \left[ \sqrt{\frac{\lambda_1}{\Delta} \cdot \frac{2}{V\pi\eta}} \exp\left(-\frac{V_g}{2kT}\right) - \frac{1}{2} \right]^3 \quad (31)$$

These formulas yield the values of  $r_{cr}$  and  $g_{cr}$  for two extreme cases of a two-phase flow: when the relative velocity between vapor and droplets is low and when the thermal velocity of vapor molecules is high.

#### NOTATION

$\Delta$	is the width of potential gap;
$k$	is the Boltzmann constant;
$m_1$	is the mass of a molecule;
$n_1$	is the number of molecules per unit vapor volume;
$T$	is the absolute temperature of vapor;
$V_g$	is the energy of bond between a molecule and a complex;
$t$	is the time.

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